

A ZERO EMISSION COMBUSTION POWER PLANT FOR ENHANCED OIL RECOVERY

GÖRAN WALL^{†*}, EUGENE I. YANTOVSKII[‡]
and

LARS LINDQUIST* and JOAKIM TRYGGSTAD*

*Department of Engineering, Kristianstad University, Box 59, S-291 21 Kristianstad, Sweden, email:
Goran.Wall@hks.se

[‡]Institute for Energy Research, Russian Ac. Sci., 44/2 Vavilova St. 117333 Moscow, Russia

(Received 19 April 1993; received for publication 25 April 1995)

Abstract – We have studied an internal combustion CO₂ power plant to enhance oil recovery. The plant has air separation of O₂ for combustion and of N₂ for injection, a combustion chamber, a turbine, a compressors, a recuperator, and a cooling tower. The oil-derived gases are used to produce liquid CO₂, highly compressed N₂, process steam and, if necessary, power. No exhaust gases are released. The plant design is presented along with efficiency calculations. The plant should be of interest for offshore oil production.

INTRODUCTION

CO₂ cycles first appeared in 1940 but attracted little attention.¹ The benefits of CO₂ compared with H₂O are low condensation heat and ability to be pumped to high pressure in the liquid state with good recuperation. Drawbacks are some toxicity, corrosion effects and a low cycle temperature (~600°C) in ordinary boilers with external combustion. Even after use of internal combustion to increase the temperature, the CO₂ cycle remained unexplored.² However, the concern of reducing CO₂ emissions to atmosphere has brought attention to fuel combustion in a mixture of O₂ and flue gases (H₂O, CO₂ or both).³⁻⁸ Efficiencies of 35-45% seem possible in spite of power use for O₂ production. The main benefit of these cycles is zero-emission, i.e. no exhaust gases. Liquid CO₂ is the only effluent.

Thermodynamic properties for internal combustion CO₂ cycles are available^{9,10} and needed economic data were estimated by the authors. To improve the economics, Steinberg and many others proposed the use of CO₂ for enhanced oil recovery (EOR). The benefit of this approach is well documented.¹¹ About 1 ton of injected CO₂ gives 0.5 ton of oil, which is admissible from a net-energy point of view. Laboratory tests have shown increased oil extraction from 54 to 96% at 120°C and 400 bar when flue gases were replaced by CO₂.¹²

We are familiar with the following processes: (i) The use of compressed N₂ to support the flow of liquid CO₂. (ii) Thermal EOR with steam or hot water as the energy carriers. (iii) The combustion of deep oil using injected O₂. The OCDOPUS (Oil Enhancement Carbon Dioxide Oxygen Power Universal Supply) plant is a suggestion for a complete EOR power plant, producing power, CO₂, N₂, O₂, process steam, and hot water (see Fig.

[†] Author for correspondence.

1). In addition to the eight processes shown in Fig. 1, cooling water is needed, e.g., sea water at an offshore plant.

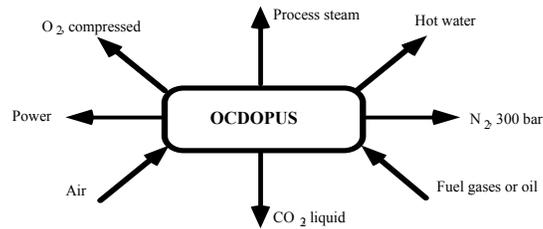


Fig. 1. The OCDOPUS plant: production and consumption.

THE OCDOPUS PLANT

The system of study is indicated by the dotted line in Fig. 2. Air is separated into O_2 and N_2 in unit 1. In a real plant, this unit will account for half the size. O_2 enters the combustion chamber 2 with recirculated CO_2 and fuel. The combustion products (mainly CO_2) expand in the turbine 8 and are cooled down in the recuperator 3 and cooling tower 4. After separation of water in unit 5, the dry CO_2 is compressed from 7 to 100 bar unit 10, which may be either an isothermal or an adiabatic process with additional recuperators.¹³

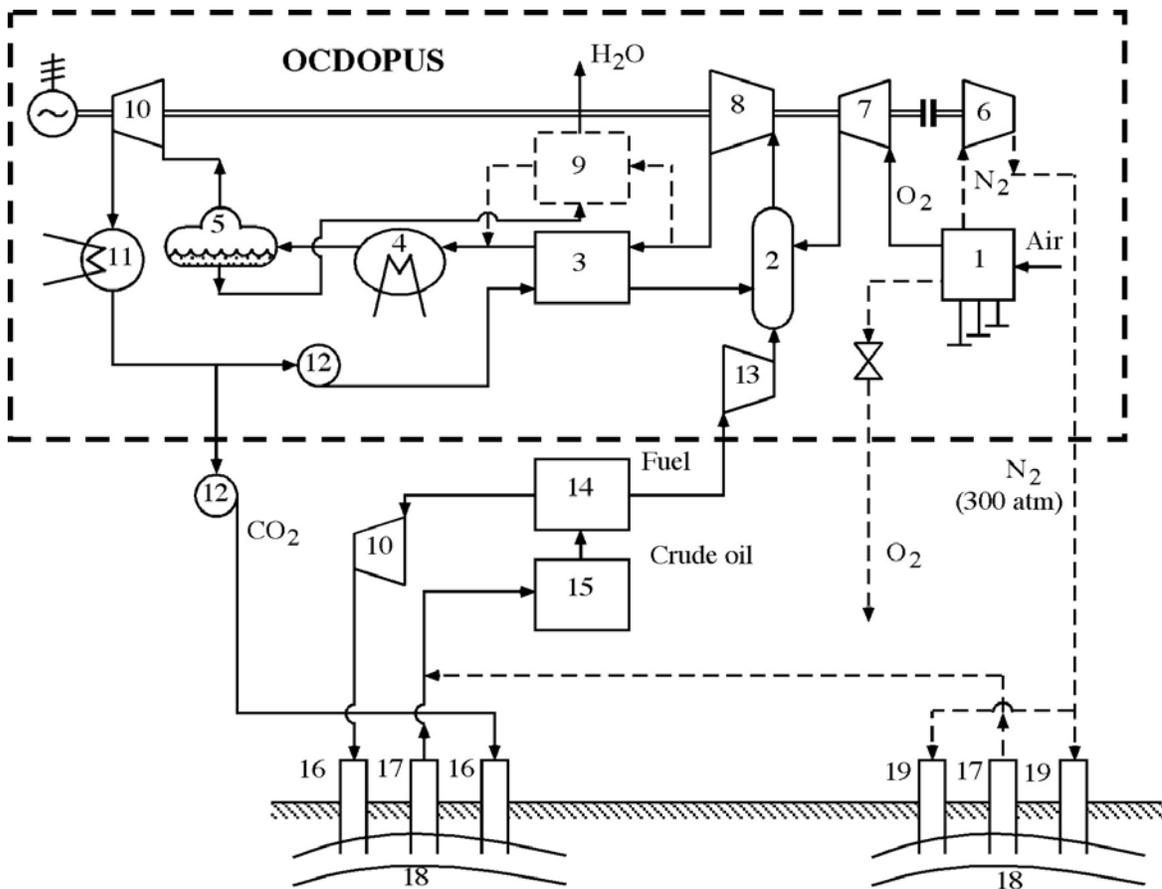


Fig. 2. Schematic of the OCDOPUS plant. 1, air separation; 2, combustion chamber; 3, recuperator; 4, cooling tower; 5, water separator; 6, N_2 compressor; 7, O_2 compressor; 8, turbine; 9, steam production; 10, CO_2 compressor; 11, CO_2 condenser; 12, CO_2 pump; 13, fuel-gas compressor; 14, CO_2 /fuel-gas separator; 15, oil/gas separator; 16, CO_2 injection well; 17, production well; 18, reservoir; 19, N_2 injection.

The CO₂ is condensed at 60 bar in unit 11, liquid CO₂ is pumped to 100 bar and returned to recuperator 3. Water from combustion may be heated in unit 9 if process steam is needed. Liquid CO₂ from combustion is injected into the well 16. The N₂ compressor 6 is attached to the shaft by a switch. When the separated N₂ is compressed and injected, the net power output equals zero.

NUMERICAL RESULTS

T-S diagrams are presented in Figs. 3 and 4. The chemical composition of the fuel (oil gases) was assumed to be C₆H₁₄. The equation for complete combustion becomes



and implies about 50 MJ/kg C₆H₁₄ with a stoichiometric coefficient of 3.6.

We use off the shelf equipment, i.e. for turbines, the maximum temperature was set equal to 1323K (1050°C). To utilize the benefits of CO₂, the pressure was set at 100 bar. The results are presented in the Table 1.

Table. 1 The results of cycle calculations for a net power of 10 MW.

	Isothermal CO ₂ compression		Adiabatic CO ₂ compression		
	Vargaftig ⁹	Altunin ¹⁰	Vargaftig ⁹	Altunin ¹⁰	
Max. temperature, K	1323	1300	1323	1300	
Recuperator drop entrance/exit, K	174/25	147/25	42/25	36/25	
Turbine work, kJ / kg	480	459	483	460	
CO ₂ compression	131.9	129.7	208.8	195.1	
Fuel-gas compression	8.5	10.0	9.24	8.7	
O ₂ compression	42.8	39.5	33.2	31.0	
Air separation	55.0	50.4	42.0	39.6	
Combustion-enthalpy rise	701.4	644.6	546.0	509.0	
Total flow rate, kg/s	43.8	45.2	53.0	53.8	
Cycle efficiency, %	34.0	35.5	35.0	36.0	
Mass fraction of the flow rate before/after combustion	Fuel	0.0141/0	0.0109/0	0.010/0	
	O ₂	0.0508/0	0.0392/0	0.037/0	
	CO ₂	0.9351/0.979	0.9403/0.9807	0.95/0.984	0.953/0.985
	H ₂ O	0/0.021	0/0.0193	0/0.016	0/0.0150
Some flows to consumers kg/s	CO ₂	1.92	1.80	1.81	1.71
	Steam	0.92	0.87	0.85	0.81
	N ₂	7	7	7	7
	300 bar zero power				

An efficiency calculation for the last column gives $(460 - 195.1 - 8.7 - 31.0 - 39.6) / 509 \approx 0.36$. The isentropic turbine efficiency was assumed to be 0.85, which is realistic for a gas turbine without cooling. We have considered both isothermal and adiabatic compression of CO₂ in unit 10, with an internal efficiency of 0.85. The isothermal, multistage, intercooled compressor consumes less power. However, according to Degtiarev,¹³ if we increase the CO₂ temperature after removing the compression heat, the entrance temperature difference in the main recuperator will decrease. This process allows us to decrease exergy losses and the total cycle efficiency is increased in spite of greater compressor work. (see the lady-boot-like cycle in Fig. 4).

Figure 5 shows the bottom part of the CO₂ cycle in greater detail. The solid line reflects adiabatic compression. For isobaric cooling, additional recuperators are used. The isothermal case is shown by the dotted line. In effect, the horizontal line consists of many teeth describing multistage compression. The enthalpy of CO₂ vapor at the end of compression is much less than at the start, which reflects non-ideal gas behavior.

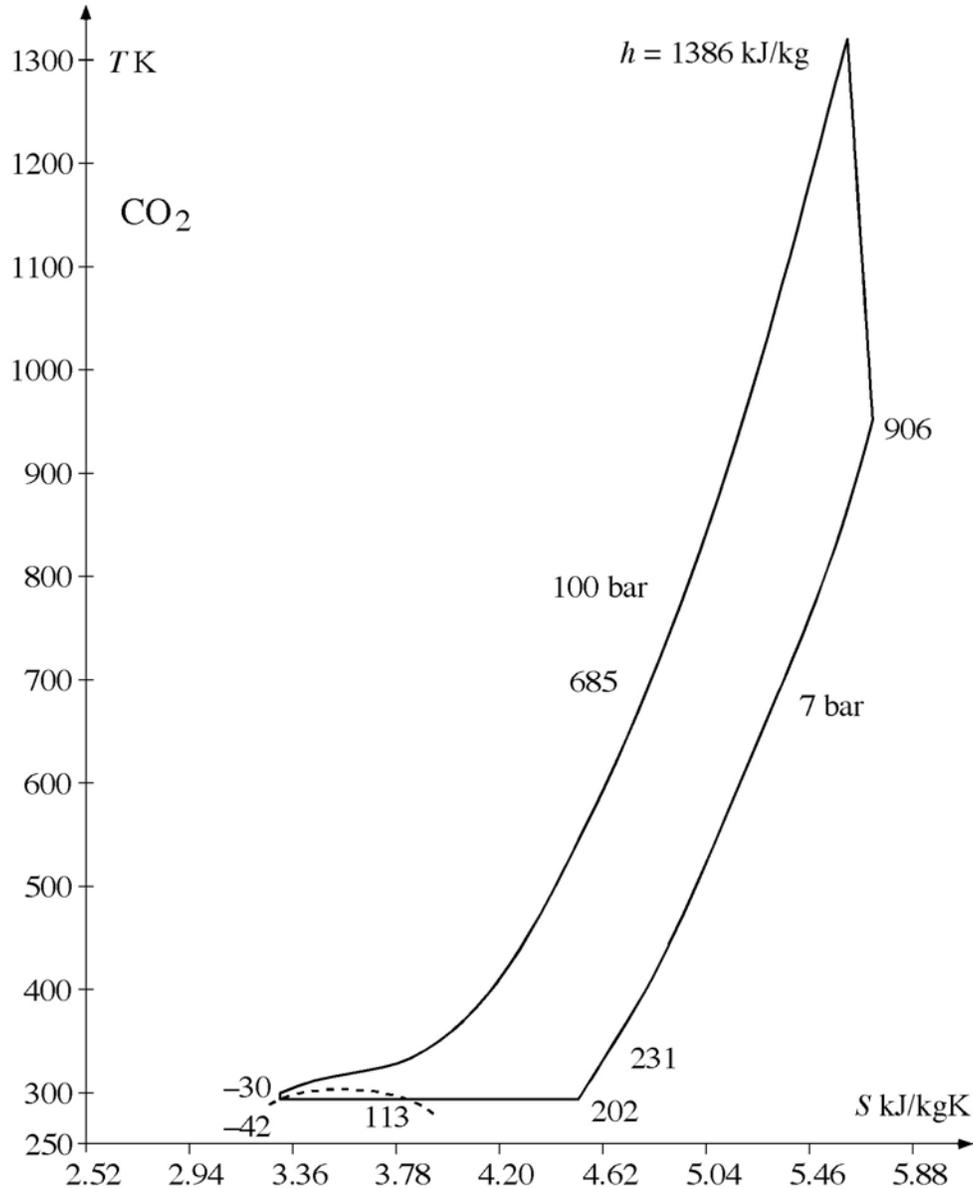


Fig. 3. T - S diagram of the cycle with isothermal compression.

In our case, the steam content is less than 2% and we therefore neglect the steam in this first study. The lack of thermodynamic tables for mixtures of CO₂ and steam makes computer simulations necessary. For CO₂, there exist discrepancies in different tables (see Table 1); the influence of these discrepancies on our results is illustrated in Table 1. Data are based on Vargaftig⁹ and Altunin.¹⁰ The evident differences are admissible first approximations.

In offshore use, the mass of the OCDOPUS plant, which is dominated by recuperator 3, may be of primary importance. In our case, the recuperator weighs about 61.4 tons, the heat transfer is 29.1 MW, and the surface area is 5990 m². The masses of the power plant and of the air-separation unit are estimated to be 100 tons each, i.e. the total mass is 200 tons or about 20 kg/kW. This is a representative figure for heavy-duty plants. More rigorous calculations should be performed in the future.

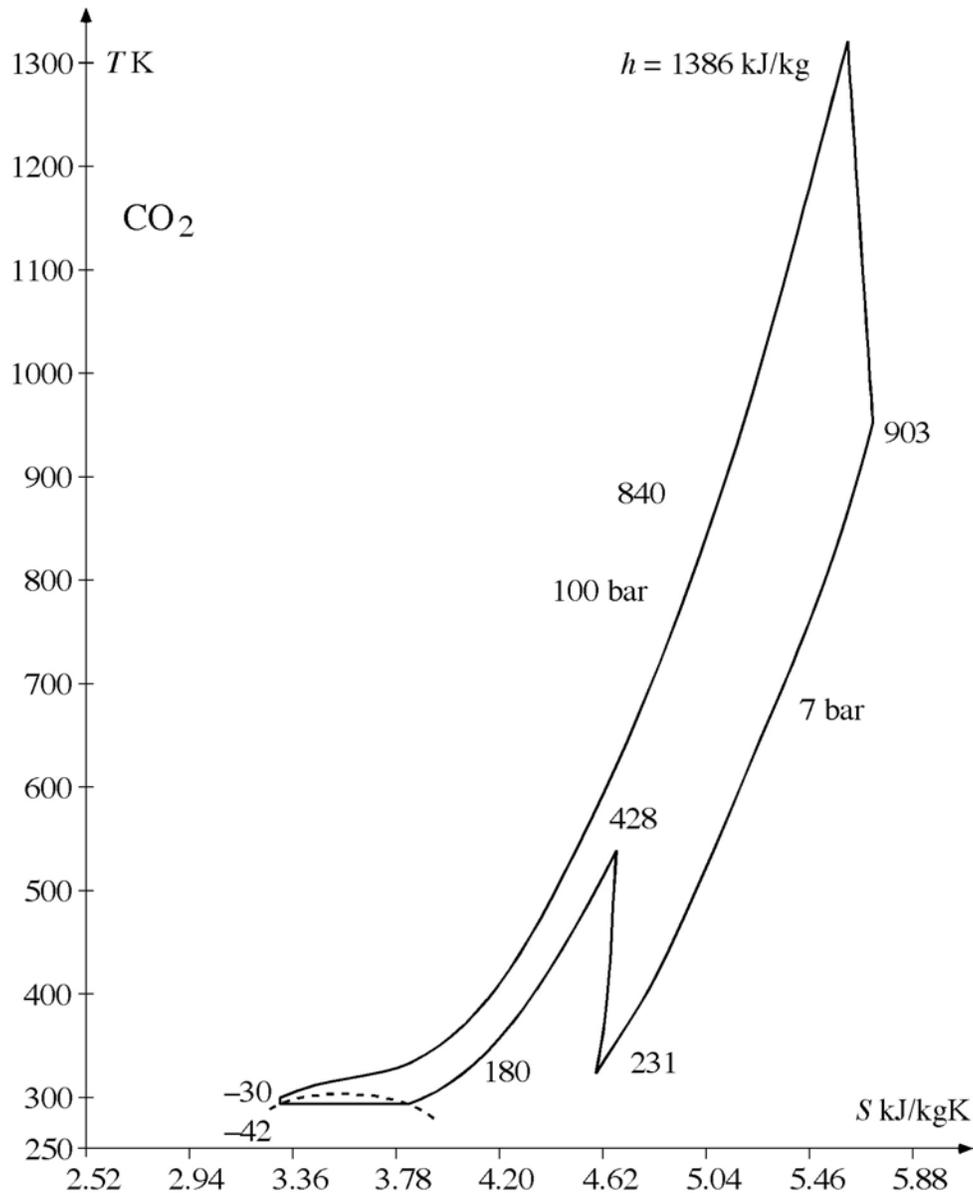


Fig. 4. T - S diagram of the cycle with adiabatic compression and additional recuperators.

CONCLUSIONS

The preliminary study of the OCDOPUS concept have shown that it is a promising concept and merits further studies. With a temperature at the turbine inlet of 1050°C, a pressure range of 7 to 100 bars, and a turbine efficiency of 85%, the efficiency becomes about 35%, and no exhaust gases are released from the plant. If the prediction of 10:1 oil-recovery to CO₂-injection ratio is valid, daily extraction of 1000 tons of crude oil is

possible; if the ratio is only 0.5:1 extraction becomes 50 tons. The daily fuel consumption (0.538 kg/s) of the 10 MW plant is just 50 tons. Therefore, a ratio of 0.5:1 is admissible when gaseous fuel is used and prohibitively low in case of crude oil combustion.

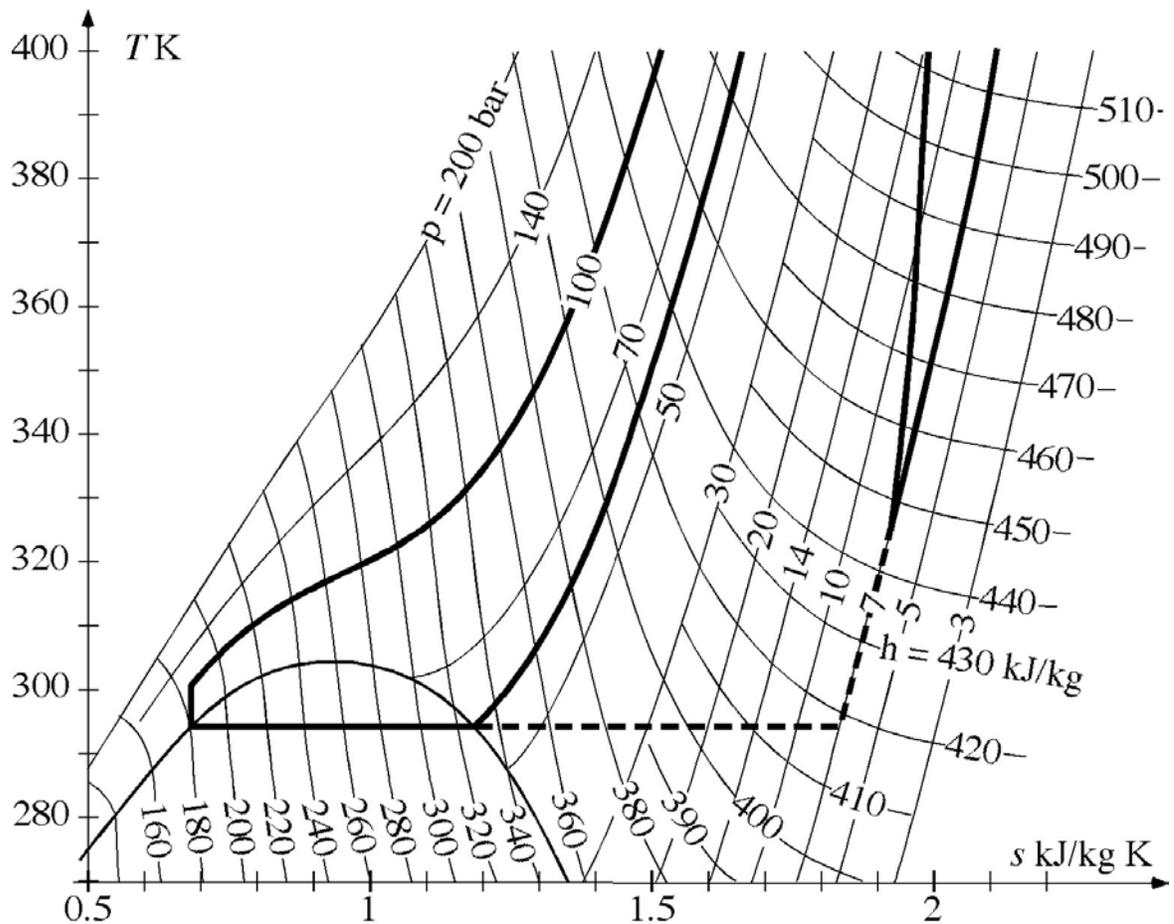


Fig. 5. T-S diagram of the cycle with adiabatic compression and additional recuperators.

REFERENCES

1. D. P. Hochstein, *Soviet Boiler and Turbine Construction* (in Russian), No. 10, 420 (1940).
2. V. L. Degtiarev and V. P. Gribovski, "Carbon Dioxide Semi-Closed Power Plant," *Bullet. of Inventions* (Nov. 12, 1971).
3. P. Pechtl, *Erdöl und Kohle Petrochemie*, No. 4, 159 (1991).
4. E. I. Yantovskii, "The Thermodynamics of Fuel-Fired Power Plants without Exhaust Gases," World Clean Energy Conf. CMDC, Geneva (Nov. 4-7, 1991).
5. J. De Ruyck, *Energy Conversion and Mgmt.* **33**, 397 (1992).
6. P. van Steenderen, "Carbon Dioxide Recovery from Coal Gas and Natural Gas Fired Combined Cycle Power Plants by Combustion in Pure Oxygen and Recycled Carbon Dioxide," COMPRIMO Consulting Services BV, information for participants at the First Intern. Conf. on CO₂ Removal, 4-6 March, Amsterdam (1992).
7. O. Bolland and S. Saether, *Energy Conversion and Mgmt.* **33**, 467 (1992).
8. T. Holt and E. Lindeberg, *Energy Conversion and Mgmt.* **33**, 595 (1992).
9. N. B. Vargaftig, *Handbook on Thermophysical Properties of Gases and Liquids* (in Russian), Phymathgiz, Moscow (1963).
10. V. V. Altunin, *Thermophysical Properties of Carbon Dioxide* (in Russian), Standard Publishers, Moscow (1975).

11. The Economic Commission for Europe and Energy Conversion, "Recent Experience and Prospects. Improved Recovery of Liquid and Gaseous Hydrocarbons from Underground Deposits," United Nations, NY (1980).
12. V. G. Scripka and E. S. Gervits, *Oil Production and Transport* (in Russian), No. 10, Moscow (1984).
13. V. L. Degtiarev, *Thermal Engineering*, No. 12 Moscow (1967).